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1 **The effect of the airflow rates and of the aeration mode on the respiration activity**
2 **of four organic wastes: Implications on the composting process**

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15

16 **Abstract**

17 The aim of this study was to assess the effect of the airflow and of the aeration mode on
18 the composting process of non-urban organic wastes, namely: (i) a fresh, non-digested,
19 sewage sludge (FSS), (ii) an anaerobically digested sewage sludge (ADSS), (iii) cow
20 manure (CM) and (iv) pig sludge (PS). This assessment was done using respirometric
21 indices. Two aeration modes were tested, namely: (a) a constant air flowrate set at three
22 different initial fixed airflow rates, and (b) an oxygen uptake rate (OUR)-controlled
23 airflow rate. The four wastes displayed the same behaviour namely a limited biological
24 activity at low aeration, whilst, beyond a threshold value, the increase of the airflow did
25 not significantly increase the dynamic respiration indices ($DRI_{1\text{ max}}$, $DRI_{24\text{ max}}$ and AT_4).
26 The threshold airflow rate varied among wastes and ranged from 42 NL air kg^{-1} DM h^{-1}
27 for CM and from 67 to 77 NL air kg^{-1} DM h^{-1} for FSS, ADSS and PS. Comparing the
28 two aeration modes tested (constant air flow, OUR controlled air flow), no statistically
29 significant differences were calculated between the respiration activity indices obtained
30 at those two aeration modes. These results permit to establish a general procedure to
31 measure the respiration activity avoiding any limitation by airflow, valid for urban and
32 non urban representative organic wastes. This will permit other researchers to provide
33 consistent results on this parameter. At the same time, better respiration activity results
34 can be obtained with the lowest aeration rate possible, that can be translated to energy
35 savings and other problems related to an excessive aeration rate can be avoided in full
36 scale composting plants.

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40 **Keywords:** dynamic respirometric index, oxygen uptake rate, composting, airflow,
41 biological activity.

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48 **1. Introduction**

49 Current legislation on solid waste management has highlighted the importance of
50 recycling and recovering these wastes as a sustainable management practice to
51 substitute traditional final disposal through incineration and landfilling. The alternatives
52 are biological treatments, based on composting, anaerobic digestion or both combined
53 treatments. In all cases, it is important to know the biological activity of the waste,
54 because it will determine the type of operation, the energy requirements and recovery,
55 and its exploitation costs (Barrena et al., 2011a).

56 Composting is a natural process where microorganisms decompose organic matter
57 into their simple elements. Compost, the final product, is stable and sanitized. Several
58 studies highlight the importance of establishing a reliable measure of the waste biological
59 activity and its biodegradability (Lasaridi and Stentidord (1998), Barrena et al. (2009),
60 Pognani et al. (2011)), because other chemically-based parameters such as TOC (total
61 organic carbon), COD (chemical oxygen demand), total organic matter content (OM,
62 expressed as volatile solids) and DOC (dissolved organic carbon) are not precise
63 enough because not all organic matter is biodegradable in real operation times. In
64 consequence, there would be an overestimation of its biodegradability using these

65 parameters (Barrena et al., 2009). Actually, measures of biological activity are a way to
66 have a realistic value on the overall efficiency of the biological treatment process either
67 in composting or in anaerobic digestion processes (Ponsá et al., 2008). Having a reliable
68 method to assess these indices is of crucial relevance for critical issues related to waste
69 management such as final quality and environmental impact assessment as previously
70 remarked (Colón et al., 2012; Scaglia and Adani, 2008). Although a consensus is not
71 reached yet, there are different suggested methodologies in scientific literature, all of
72 them based on biological activities.

73 Ponsá et al. (2008) found a good correlation between aerobic and anaerobic indices.
74 Barrena et al. (2009) also found a significant correlation between cumulative oxygen
75 consumption and ultimate biogas production. Both correlations were found using
76 samples from mechanical-biological treatment (MBT) plants treating municipal solid
77 wastes. This indicates that both indices can be used to express the degree of biological
78 stability. Aerobic indices were recommended for its shorter time of assay. In general,
79 aerobic respiration indices have been highlighted as the most suitable tool for
80 biodegradability and stability assessment, to monitor the process and to implement new
81 improvements (Ponsá et al., 2010a, Barrena et al., 2009). Dynamic Respiration Indices
82 (DRI) are well established (Scaglia2011?)and used in composting research because of
83 their advantages over static respiration indices or BOD with solids samples, such as the
84 presence of a continuous airflow during the measurement, that do not limit the oxygen
85 transfer through the biomass layer (Adani et al., 2003 and 2006).

86 Barrena et al. (2011b), studied the behaviour of respiration activity on different
87 wastes, classified in four groups: municipal solid wastes, wastewater sludge, manure,
88 bulking agents and other wastes. Authors observed that municipal solid wastes with higher
89 percentage of organic matter showed higher respiration ctivity. This biological activity

90 increased when studying the source-selected organic fraction of municipal solid wastes
91 (OFMSW). With regard to wastewater sludge, the anaerobic digestion process decreases
92 the respiration activity by 60-70% (Ponsá et al., 2008). Fresh wastewater sludge
93 biodegradability can change depending on the treatment applied or its origin, but
94 digested wastewater sludge is usually more homogeneous. Manure shows a moderate
95 respiration activity, far from those obtained with OFMSW and non-digested wastewater
96 sludge (Barrena et al. 2011b). Part of this activity can be lost during their storage, as a
97 part of its treatment (Bonmatí and Flotats, 2003). In summary, organic wastes from
98 different origins, organic matter content and history will present different level of
99 respiration activity. This will directly affect the aeration requirements and the
100 composting process overall performance.

101 Aeration rate is expected to have an important effect on the microbial respiration,
102 thus in biological activity and stability of the material. In Komilis and Kanellos (2012),
103 a positive correlation between the dynamic respiration index DRI_{24} and unit airflow
104 rates (range XXXX) was observed, as well as a negative correlation between CO_2 index
105 and unit airflow rate.

106 Almeida et al. (2015), studied the effect of different airflow rates (range XXXX) and
107 different aeration modes on the microbial respiration activity. Three different organic
108 wastes derived from the OFMSW were studied, using constant airflow and an OUR
109 (oxygen uptake rate) controlled airflow, which is continuously adjusted to keep the
110 oxygen uptake rate optimized (Puyuelo et al., 2010). Results showed that a constant
111 airflow below $20 \text{ L kg}^{-1} \text{ DM h}^{-1}$ limited respiration activity, while airflows above that
112 value resulted in statistically similar respiration activities.

113 Aeration conditions also influence the composting process performance in terms of
114 biodegradation rate, process time and GHG emissions from the composting process.

115 Insufficient aeration can lead to oxygen limitations that lead to poor biodegradation
116 rates. Excess of aeration can eventually cause major water losses and hamper moisture
117 control (Ruggieri et al., 2008). It is considered as one of the most important factors, as
118 insufficient aeration can lead to anaerobic condition, resulting in an increase of CH₄
119 emissions (Jiang et al. 2011). Jiang et al. (2015) observed that higher aeration rates
120 increased NH₃ and N₂O losses, but showed a higher mitigation on CH₄ emissions, when
121 composting pig feces.

122 The aim of this study is to evaluate the effect of different airflow rates and different
123 aeration modes on the microbial respiration using different organic wastes via several
124 DRI. Four parameters were analysed: DRI₁ (1-hour Dynamic Respirometric Index
125 average), DRI₂₄ (24-hours Dynamic Respirometric Index average), AT₄ (cumulative
126 oxygen consumed in four days) and lag phase. Four non-urban type organic wastes were
127 tested and their performance was compared with the organic fraction of municipal solid
128 waste tested by Almeida et al. (2015). Wastes used in this study were selected because
129 of their high production volume. For instance, Catalonia region, with 7 million
130 inhabitants, produces per year 2 million tons of wastewater sludge on dry mass basis
131 and 20 million tons of manure, being cow and pig manure the main components. In
132 consequence, these materials have been selected as representative wastes to illustrate the
133 different typology of non-urban and livestock organic wastes (Campos et al. 2004,
134 Ministerio de Agricultura y Pesca, Alimentación y Medio Ambiente, 2012). Two
135 aeration regimes were used: i) a constant unit airflow rate and ii) a continuous and
136 variable airflow rate as adjusted by the OUR controller. Results obtained will help to
137 establish the necessary amount of air in order to measure with accuracy the microbial
138 respiration in the laboratory. In addition, results will aid to calculate the aeration

139 necessary at full scale to provide an effective stabilization for different types of
140 agricultural and industrial organic wastes.

141

142 **2. Materials and Methods**

143

144 2.1. Organic wastes

145 Four different non-urban organic wastes were used in this work:

146 (i) a fresh, non-digested, sewage sludge (FSS) from the wastewater treatment plant
147 in Olot (Girona, Spain),

148 (ii) an anaerobic digested sewage sludge (ADSS) from the wastewater treatment
149 plant in Sabadell (Barcelona),

150 (iii) cow manure (CM) obtained from a local farm in Catalunya, and

151 (iv) pig slurry (PS) from a farm of Vic (Barcelona).

152 FSS and ADSS were sampled in their respectively wastewater treatment plant, while
153 cow manure and pig slurry were sampled on a storage pile and a storage pond,
154 respectively.

155 . Table 1 shows their characterization.

156

157 2.2. Respiration tests

158 90 g of sample from each of the aforementioned substrates were used in each
159 individual respiration run (i.e. per replicate). To ensure a good porosity of the material,
160 9 g of inert bulking agent were added and manually mixed with FSS, ADSS and PS.
161 The bulking agent consisted of small pieces (1 x 2 cm) of dishclothes (Spontex)
162 (Puyuelo et al., 2011). All tests were run in triplicate.

163 The dynamic respirometer consisted of 12 500 mL custom made reactors, as
 164 described elsewhere (Ponsá et al, 2010b), used to measure the respiration activity.
 165 Briefly, the individual waste sample or mixture was placed in each 500 mL reactor.
 166 Each reactor consisted of an Erlenmeyer flask, containing a plastic net to support the
 167 organic waste and to provide an air distribution chamber, placed in a water bath at 37°C
 168 (Fig. 1). Airflow to the reactor was adjusted by means of an airflow controller
 169 (Bronkhorst Hitec, The Netherlands). Air was passed through a humidifier at the same
 170 temperature of the reactor to avoid water losses and moisture changes. Exhaust air from
 171 the reactor was sent to a dehumidification water trap and later to an oxygen sensor. Air
 172 flow meters and oxygen sensor were connected to a data acquisition system to
 173 continuously record the on-line calculations of the selected respiration indices.

174

175 2.3. Respiration Indices

176 Dynamic respiration index (DRI) can be calculated from oxygen and airflow data for
 177 a given time (Eq. [1]) (Ponsá et al., 2010b).

$$178 \quad DRI_t = \frac{(O_{2,i} - O_{2,o}) \cdot F \cdot 31.98 \cdot 60 \cdot 1000^a}{1000^b \cdot 22.4 \cdot DM} \quad \text{Eq. [1]}$$

179 Where: DRI_t , dynamic respiration index for a given time t ($\text{mg O}_2 \text{ g}^{-1} \text{ DM h}^{-1}$); ($O_{2,i} -$
 180 $O_{2,o}$), difference in oxygen content between airflow in and out the reactor at that given
 181 time, molar fraction; F, volumetric airflow measured under normal conditions (1 atm
 182 and 273 K) (mL min^{-1}); 31.98, oxygen molecular weight (g mol^{-1}); 60, conversion factor
 183 (minutes h^{-1}); 1000^a , conversion factor (mg g^{-1}); 1000^b , conversion factor (mL L^{-1});
 184 22.4, volume occupied by one mol of ideal gas under normal conditions (L); DM, dry
 185 mass of the substrate under study that is loaded in the reactor (g).

186 Total cumulative oxygen consumption (AT_u) was determined through the numerical
187 integration of the continuous DRI_t data obtained. It was calculated according Eq. [2]
188 (Puyuelo et al., 2010).

$$189 \quad AT_u = \int_0^t DRI_t dt \quad \text{Eq. [2]}$$

190 Where AT_u , is the total oxygen consumption between time 0 and t beyond the initial
191 lag phase ($\text{g O}_2 \text{ g}^{-1} \text{ DM}$); t, the final experimental time (h); DRI_t , dynamic respiration
192 index for a given time t ($\text{mg O}_2 \text{ g}^{-1} \text{ DM h}^{-1}$).

193 The three respiration indices studied in this work were: (a) DRI_1 , which is the
194 average of the instantaneous oxygen uptake rate during a 1-hour period, (b) DRI_{24} ,
195 which is the average of the instantaneous oxygen uptake rate during the most intense 24
196 hours of biological activity (Barrena et al., 2009) and (c) AT_4 , which is the total oxygen
197 consumed over a 4 day period beyond the initial lag time (Almeria et al., 2015).
198 Respiration tests were run for 5 to 7 days so AT_4 could be calculated. Another important
199 parameter calculated was the lag phase (h). Lag phase is finished when the observed
200 respiration activity is 25% of the value results in the region of largest increase in oxygen
201 consumption within the first four days (Federal Government of Germany, 2001).

202

203 2.4. Aeration modes

204 In the constant airflow regime, airflow was adjusted to maintain the initial value
205 throughout the experiment. In the OUR control airflow regime, airflow was
206 continuously adjusted to optimize oxygen uptake rate by an automatic controller.
207 Puyuelo et al., (2010) developed and optimized the algorithm for this new control
208 strategy and validated it in the composting of different wastes. Almeira et al., (2015)
209 successfully used this same OUR-controller in respiration tests. The OUR controller

210 compares the variations of different OUR measures in different cycles according to the
211 airflow applied and establishes an airflow according to the measure and the comparison
212 of the flow applied between two consecutive cycles. A safety secondary loop is included
213 to ensure that the oxygen level does not fall below 5%. The oxygen level was always
214 over 15% in the experiments reported in this work. This strategy has demonstrated to
215 be the most suitable in terms of lower air consumption, final biological stability and
216 process gas emissions (Puyuelo et al., 2014). The use of two methods of aeration were
217 selected for observe the difference between a limited oxygen system (constant airflow
218 regime) and a non-limited oxygen system (OUR control airflow regime).

219

220 2.5. Experimental design and statistical analysis

221 Three constant airflows were tested for each sample: 5 ml min⁻¹, 15 ml min⁻¹ and 30
222 ml min⁻¹. An additional not-constant aeration strategy was included based on the OUR-
223 controller. Table 2 shows each airflow expressed as NL air kg⁻¹ DM h⁻¹ to express the
224 volumetric flow in more easily extrapolated units. These ranges were selected to cover a
225 wide range of aeration values according to the expected biological activity of the five
226 substrates. The experimental period was 5-7 days. Three independent replications per
227 treatment were done. Statistical analysis was performed with basic ANOVA techniques
228 while pairwise comparisons were based on the Tukey test (at p < 0.05). Statistics were
229 performed with MINITABTM V17 .

230

231 **3. Results and Discussion**

232 The characterisation of the organic wastes is shown in Table 1. While organic matter
233 content is similar for all wastes tested, the percentage of moisture varies according to
234 the type of waste. CM presents a lower water content than the rest of the wastes (FSS,

235 ADSS, PS). Thus the same constant volumetric airflow represents a lower specific
236 aeration rate for CM than for the rest of the samples (Table 2). The moisture of the
237 samples at the end of the respiration test was analysed. No water loss was observed
238 according to the respirometer configuration described. Regarding pH, the materials were
239 slightly alkaline, confirming that no acidification occurred during storage (Rudrum,
240 2005).

241

242 3.1. Oxygen uptake profiles

243 Figure 2 presents one full respiration profile for each waste under a constant aeration
244 rate of 15 mL min⁻¹. Similar profiles were obtained for each waste in all the experiments
245 regardless the applied airflow. According to Fig. 2, the OUR profile of the four wastes
246 followed the typical ascent to a peak value, which usually coincides with the rise of the
247 temperature in the real composting process (Puyuelo et al., 2010), and is followed by a
248 progressive decrease. The OUR peaks in the first 5-10 hours for FSS, ADSS and PS,
249 and later in the case of CM, at around 20h of process. In the case of pig slurry only, a
250 second peak was observed. Dabert et al. (2010) and Esteve et al. (2009) reported that
251 successive respiration peaks could occur but would have nothing to do with
252 environmental conditions, such as moisture or temperature. Denes et al. (2015) led the
253 hypothesis that the second respiration peak corresponds to the growth of a different
254 microbial community and occurs when the most recalcitrant part (slowly hydrolysed)
255 becomes available to biodegradation. Another fact to remark is that in all those
256 homogeneous wastes, lag phase was very brief or virtually non-existent.

257

258 3.2. Effect of airflow rate on respiration indices

259 Figures 3 to 6 describe the effect of different airflow rates on three main respiration
260 indices (DRI_1 , DRI_{24} and AT_4) and on the lag phase. Two statistical analyses were
261 performed with the goals to a) compare the behaviour of each individual waste under
262 the different aeration rates (controlled, constant) and b) to compare the behaviour of all
263 wastes tested under different aeration rates. Both analyses were based on ANOVA
264 principles.

265 Figure 3 presents the DRI_1 for the four materials under the 4 different aeration
266 regimes. In all cases, respiration indices increased when the feeding airflow increased,
267 as had been also observed by Komilis and Kanellos (2012). The difference was
268 significant when increasing airflow from 5 to 15 mL min^{-1} . However further rise to 30
269 mL min^{-1} did not significantly increase the DRI_1 . This is in accordance with results
270 reported by Almeida et al. (2015) who had used the organic fraction of municipal solid
271 wastes (fresh, partially degraded and composted) in their experiments. The OUR-based
272 aeration strategy led to higher DRI_1 values in all cases, although no statistically
273 different. On the contrary, Almeida et al. (2015) reported a significant increase in
274 respiration indices under the OUR aeration mode when analysing OFMSW and
275 compost.

276 Same behaviour was observed for DRI_1 , DRI_{24} and AT_4 (Figures 3, 4 and 5). That is,
277 increasing aeration upon a given threshold did not further improve the respiration
278 indices. 5 mL min^{-1} was insufficient, probably due to mass transfer limitations within
279 the reactor. Increasing to 15 mL min^{-1} or higher aeration rates favoured air distribution
280 in the reactor and thus enhanced the oxygen uptake rate. This means that maximum
281 respiration activity is reached around 15 mL min^{-1} and there is no need for an extra air
282 supply. Furthermore, higher aeration rates lead to higher energy consumptions and
283 process emissions. For instance, Jiang et al., (2015) reported an increase of NH_3 and

284 N₂O emission when increasing aeration rates in the composting process. Colón et al.
285 (2012) quantified the emissions related to energy consumption in providing aeration. In
286 all cases, OUR aeration mode ensured a good respiration result. In this sense, this
287 strategy is advisable to avoid aeration limitations when using a new and unknown
288 waste.

289 Table 3 summarizes the results obtained and presents the threshold specific aeration
290 rate expressed as NL kg⁻¹ DM h⁻¹. As expected, fresh sewage sludge exhibited a higher
291 respiration activity than the anaerobic digested sewage sludge, since, during anaerobic
292 digestion, biodegradable organic matter is transformed to biogas. Cow manure and pig
293 slurry showed similar results to ADSS, as these three wastes are partially stabilised
294 materials (Barrena et al., 2011a and 2011b). These are expected results, because we
295 observe that wastes that are more biologically active, such as fresh sewage sludge, to
296 present a high respiration activity; in consequence, high DRI₁, DRI₂₄ and AT₄ values are
297 observed as well. It was also expected that the previously anaerobically digested sludge
298 would present a lower respiration activity compared to fresh sewage sludge (50% lower
299 activity). This was true, since that waste has been already stabilized during the
300 anaerobic digestion process and it lost respiration capacity. This observation agrees with
301 Barrena et al. (2011b). In the case of cow manure and pig slurry, the relatively low
302 respiration activity (as compared to sludge) was expected, because although these are
303 normally biologically active wastes, they can lose respiration activity during their
304 storage on farms (Bonmatí and Flotats, 2003). Specific air flows are slightly different
305 (Table 3) due to the 10% difference in moisture content of the materials (76.2-86.7%,
306 Table 1). Finally, comparing our results to those obtained by Almeida et al., (2015) that
307 had used only the organic fraction of municipal solid waste (OFMSW), it can be noticed
308 that although OFMSW is a very biologically active waste, its response was similar to

309 that of ADSS, CM and PS. Specifically, indices obtained for OFMSW under constant
310 aeration were: 3.2 g O₂ kg⁻¹ DM h⁻¹ (DRI₁), 3.1 g O₂ kg⁻¹ DM h⁻¹ (DRI₂₄) and 228.2 g
311 O₂ kg⁻¹ DM (AT₄) (Almeira et al., 2015) which are values similar to the ones obtained
312 here for ADSS, CM and PS.

313 According to the results, we can categorize these organic materials according to their
314 biodegradability, as had been proposed by Barrena et al. (2011b). Fresh sewage sludge
315 would be categorized as a highly biodegradable waste, due to its respiration activity that
316 is higher than 5 g O₂ kg⁻¹ DM h⁻¹, while the anaerobic digested sewage sludge, cow
317 manure and pig slurry would be categorized as moderately biodegradable wastes, given
318 the fact that their respiration activity is between 2 and 5 g O₂ kg⁻¹ DM h⁻¹.

319 The purpose of the composting process is to stabilize and sanitize urban and non-
320 urban wastes. The European Commission uses parameters such as AT₄ or DRI to define
321 if the material is completely stabilized or not. According to proposals suggested by the
322 European Commission, a waste can be characterized as well stabilized if AT₄ is below
323 10 g O₂ kg⁻¹ DM or if DRI is below 1 g O₂ kg⁻¹ DM (European Commission, 2001).

324 Fig. 6 presents the lag phase observed in the respirometric tests for the four
325 materials. Lag time was reduced when increasing the aeration rate from 5 to 15 and to
326 30 mL min⁻¹ in all cases. The OUR aeration mode led to slightly higher lag times.

327 When comparing the two aeration modes, the constant airflow and the airflow with
328 OUR control, we can observe that there is not a statistically significant different
329 response between 15 and 30 ml min⁻¹ airflow mode and with the airflow OUR control
330 mode. The value that wastes achieve in 15 and 30 ml min⁻¹ is the same value that is
331 achieved with an airflow OUR control mode. So airflows below 15 ml min⁻¹ appear to
332 limit microbial respiration activity. In Almeira et al. (2015) similar results had been

333 obtained, since a constant airflow below $20 \text{ L kg}^{-1} \text{ DM h}$ had been found to limit the
334 microbial respiration activity in municipal solid wastes.

335

336 **4. Conclusions**

337 In conclusion, the study demonstrated the following:

338 • There is not a continuous linear relation between the airflow supply and the
339 respiration activity. Actually, there is a flowrate threshold, above which any further
340 increase does not affect biological activity. This threshold is achieved at a constant
341 airflow of $67 \text{ NL air kg}^{-1} \text{ DM h}^{-1}$, in the case of FSS and ADSS, $42 \text{ NL kg}^{-1} \text{ DM h}^{-1}$
342 in the case of CM and $77 \text{ NL kg}^{-1} \text{ DM h}^{-1}$ in the case of PS. Below those specific air
343 flowrate thresholds, the respiration activity is limited and is positively correlated to
344 the air flowrate.

345 • The DRI_{24} ranged from 2 to $6 \text{ g O}_2 \text{ kg}^{-1} \text{ DM h}^{-1}$. FSS was the substrate with the
346 highest respiration activity, followed by the cow manure. No clear correlation
347 between respiration activity and organic matter content can be deduced from this
348 work.

349 • Comparing the two aeration modes tested (constant air flow, OUR controlled air
350 flow), no significant difference is observed between the respiration activity indices
351 obtained by those two aeration modes.

352 • Comparing urban waste (from a previous study) and non-urban wastes, non-urban
353 wastes were more biologically active, with FSS being the most biologically active
354 one among all.

355 These results determine the procedure for a proper measurement of the respiration
356 activity in organic wastes, allowing other researchers to provide consistent results on
357 this parameter. This has implications in providing a reliable measure of biological

358 stability; assessing the proper aeration in composting facilities in the full scale
359 improving the process economics; and avoiding environmental impacts of the
360 composting process and the use of the final product.

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Tables

Table 1. Initial moisture, organic matter and pH of the four substrates tested (mean \pm stdev).

Substrate	Moisture (% wb)	Organic matter (% db)	pH
FSS	85.0 \pm 1	85.0 \pm 1	7.51
ADSS	85.3 \pm 0.03	78.4 \pm 0.1	8.21
CM	76.2 \pm 0.1	91.9 \pm 0.2	7.98
PS	86.7 \pm 0.2	83.0 \pm 7	8.14

FSS: fresh sewage sludge; ADSS: anaerobically digested sewage sludge; CM: cow manure; PS: pig sludge.

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Table 2. Specific airflow achieved (in NL air kg⁻¹ DM h⁻¹) at the two aeration modes (constant, OUR controlled).

Waste	Constant airflow (5 ml min ⁻¹)	Constant airflow (15 ml min ⁻¹)	Constant airflow (30 ml min ⁻¹)	OUR-controlled airflow
FSS	22.2	66.7	133.3	55 – 238
ADSS	22.2	66.7	133.3	64 – 336
CM	13.9	41.7	83.3	40 – 187
PS	25.6	76.9	153.8	75 – 511

FSS: fresh sewage sludge; ADSS: anaerobically digested sewage sludge; CM: cow manure; PS: pig sludge

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Table 3. Summary of respirometric indices obtained at the threshold airflow of 15 mL min⁻¹.

Substrate	Threshold airflow (NL kg ⁻¹ DM h ⁻¹)	DRI _{1 max}	DRI _{24 max}	AT ₄	Lag phase
FSS	67	6.4 ± 0.9 ^B	4.9 ± 0.7 ^E	312 ± 45 ^H	0.9 ± 0.2 ^{LM}
ADSS	67	3.7 ± 0.4 ^C	2.5 ± 0.3 ^{FD}	158 ± 25 ^I	0.7 ± 0.6 ^M
CM	42	3.7 ± 0.6 ^C	3.3 ± 0.6 ^F	241 ± 44 ^J	1.2 ± 0.1 ^{LM}
PS	77	4.2 ± 0.5 ^C	3.2 ± 0.5 ^F	209 ± 31 ^{GI}	1.5 ± 0.2 ^L

FSS, fresh sewage sludge; ADSS, anaerobic digested sewage sludge; CM, cow manure;

PS, pig sludge; means with the same letter at statistically similar at p < 0.05.

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549 **Legends to Figures**

550

551 **Figure 1.** Experimental setup of the dynamic respiration measurement system.

552

553 **Figure 2.** Comparison of different oxygen consumption profiles of: a) FSS (fresh
554 sewage sludge) and ADSS (anaerobically digested sewage sludge) and b) CM (cow
555 manure) and PS (pig sludge).

556

557 **Figure 3.** Comparison of maximum 1-hour average Dynamic Respiration Indices ($DRI_{1\text{ max}}$)
558 versus 5, 15 and 30 ml min^{-1} constant airflow rate and an Oxygen Uptake rate
559 (OUR) airflow control, obtained by FSS (fresh sewage sludge), ADSS (anaerobically
560 digested sewage sludge), CM (cow manure) and PS (pig sludge). Same letters indicate
561 statistically similar means at $p < 0.05$ (comparison is made among all means shown in
562 the graph).

563

564 **Figure 4.** Comparison of maximum 24-hour average Dynamic Respiration Indices
565 ($DRI_{24\text{ max}}$) versus 5, 15 and 30 ml min^{-1} constant airflow rate and an Oxygen Uptake
566 Rate (OUR) airflow control, obtained by FSS (fresh sewage sludge), ADSS
567 (anaerobically digested sewage sludge), CM (cow manure) and PS (pig sludge). Same
568 letters indicate statistically similar means at $p < 0.05$ (comparison is made among all
569 means shown in the graph).

570

571 **Figure 5.** Comparison of total oxygen consumed over a 4 day period beyond the initial
572 lag phase (AT_4) versus 5, 15 and 30 ml min^{-1} constant airflow rate and an Oxygen
573 Uptake Rate (OUR) airflow control, obtained of FSS (fresh sewage sludge), ADSS
574 (anaerobic digested sewage sludge), CM (cow manure) and PS (pig sludge). Same
575 letters indicate statistically similar means at $p < 0.05$ (comparison is made among all
576 means shown in the graph).

577

578 **Figure 6.** Comparison of lag phase (h), versus 5, 15 and 30 ml min^{-1} constant airflow
579 rate and an Oxygen Uptake Rate (OUR) airflow control, obtained of FSS (fresh sewage
580 sludge), ADSS (anaerobic digested sewage sludge), CM (cow manure) and PS (pig
581 sludge). Same letters indicate statistically similar means at $p < 0.05$ (comparison is
582 made among all means shown in the graph).

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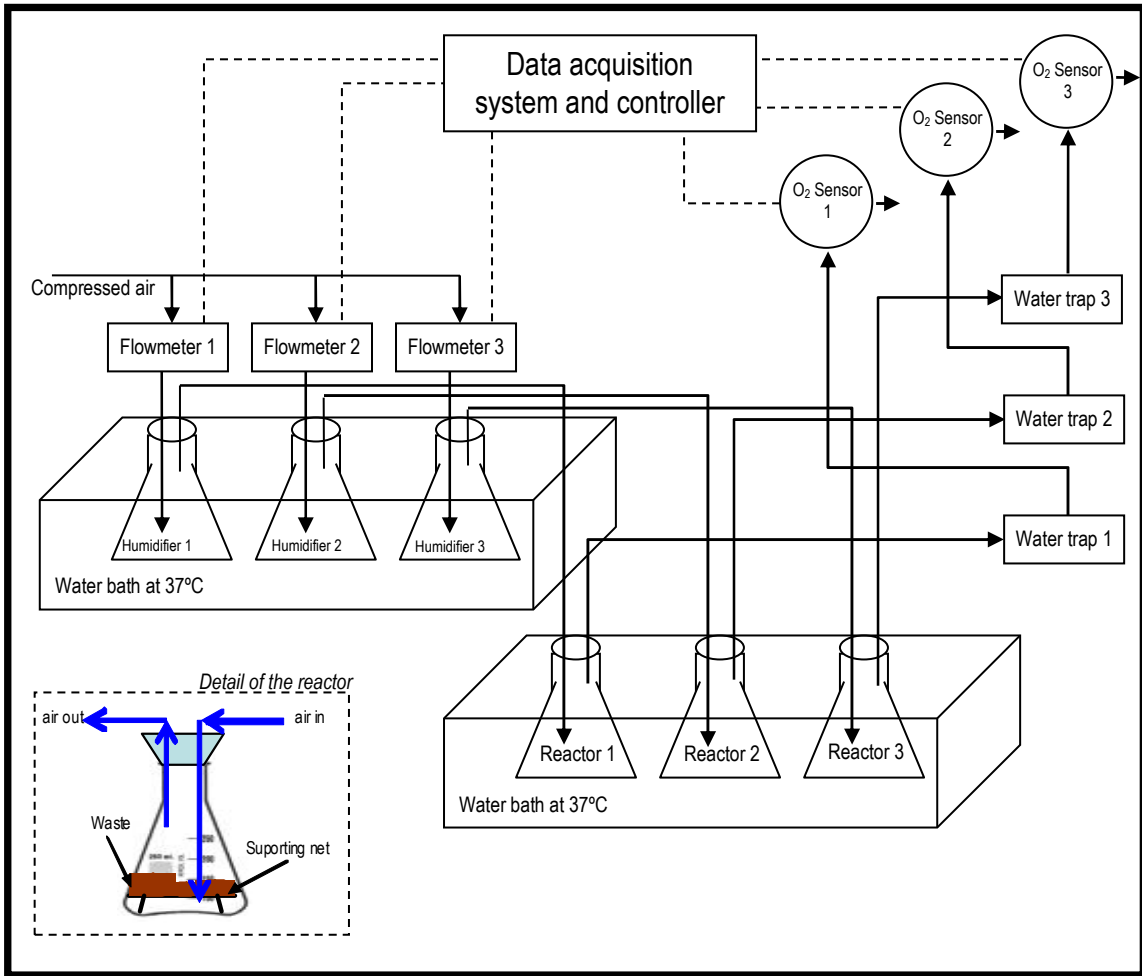
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590 FIGURE 1



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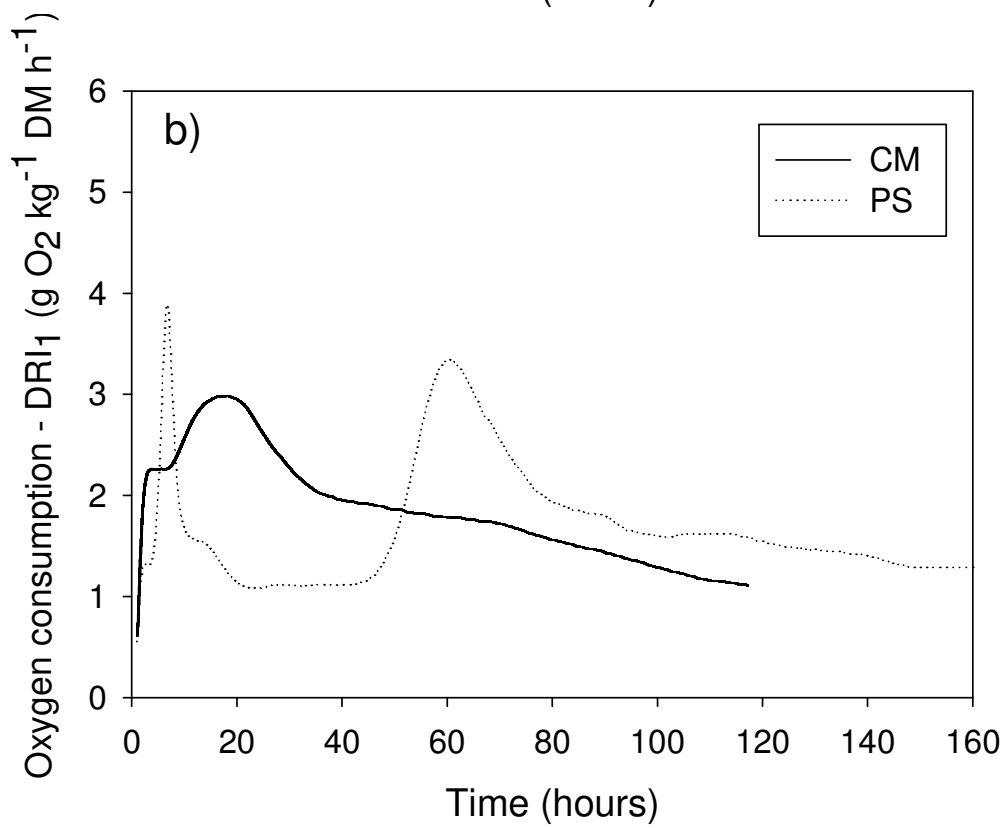
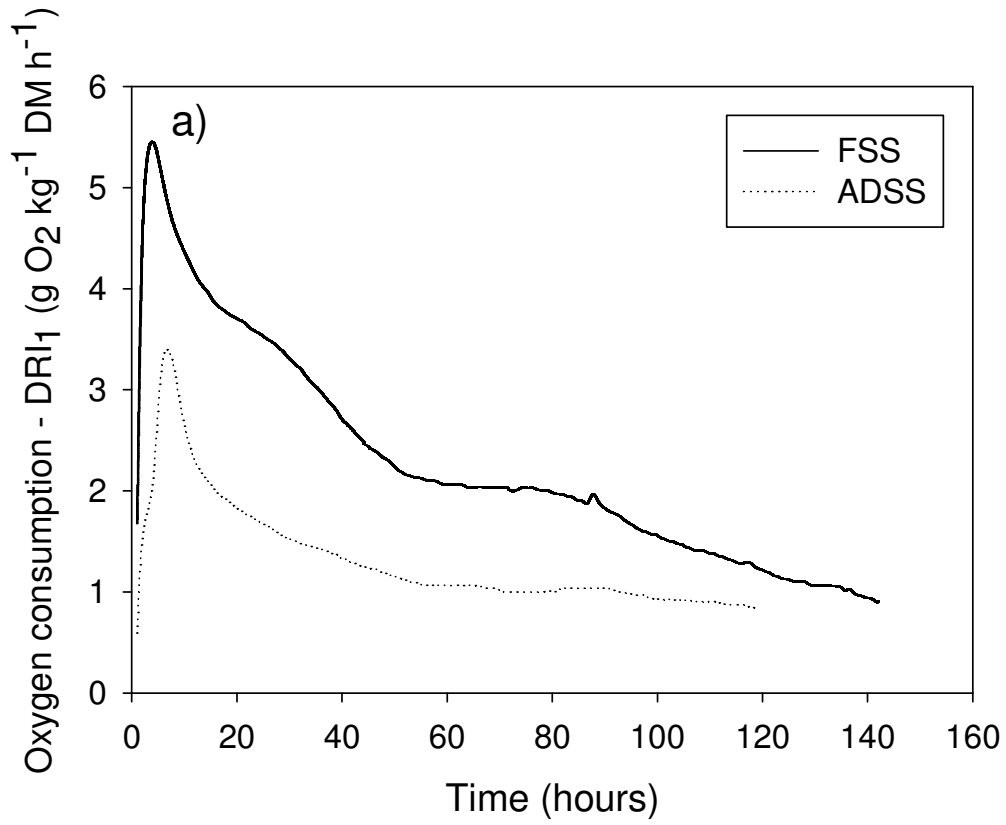
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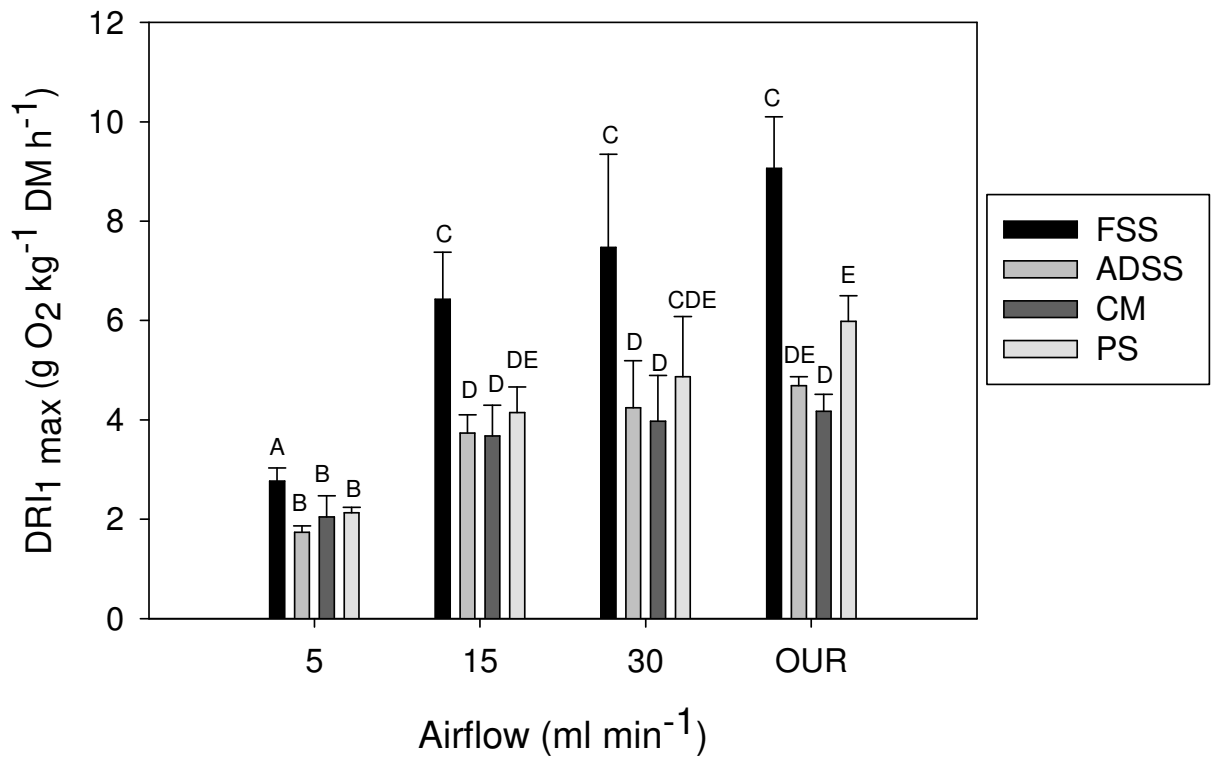
600 FIGURE 2



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635 FIGURE 3



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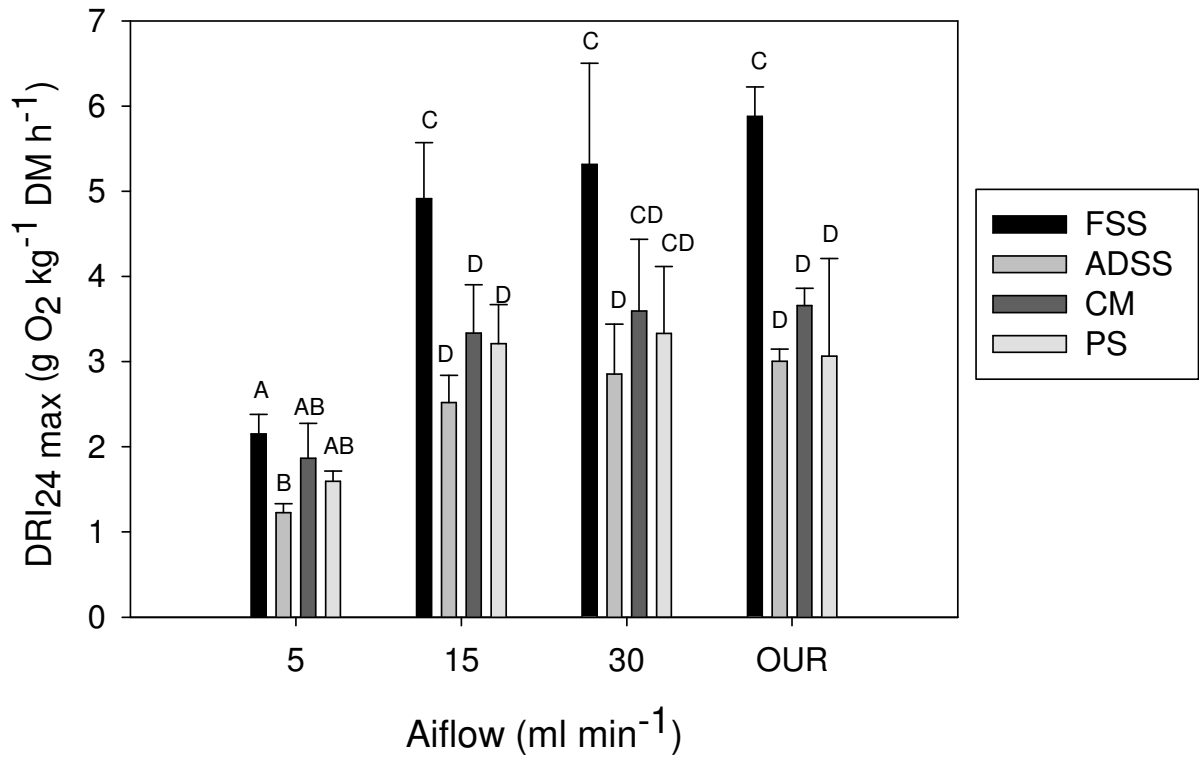
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651 FIGURE 4



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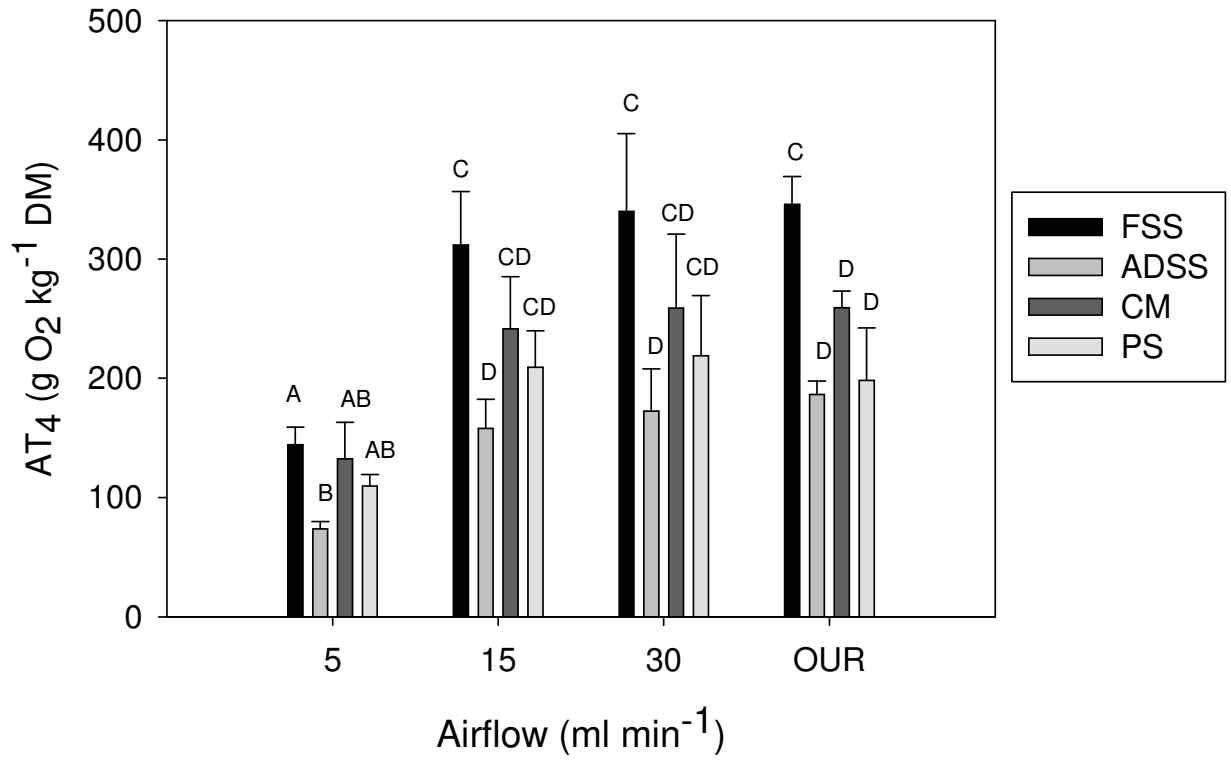
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667 FIGURE 5



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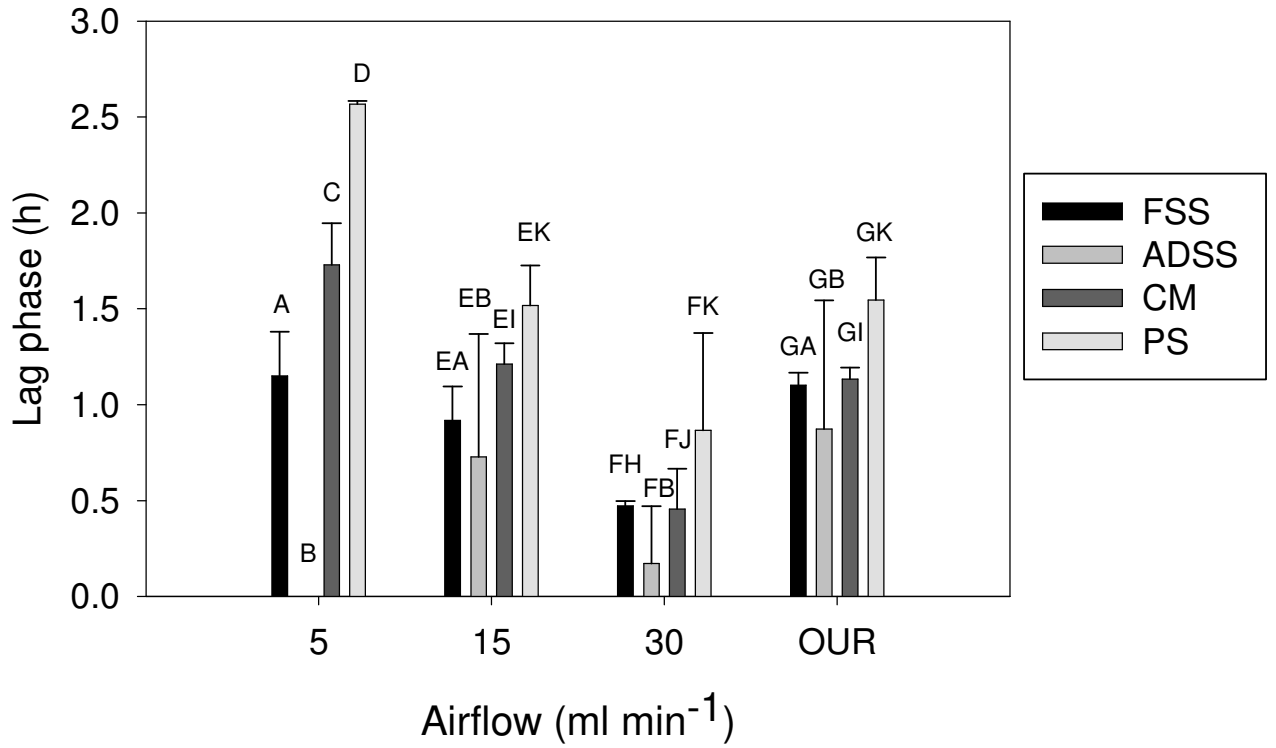
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683 FIGURE 6



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