

# BIOPROCESS DESIGN FOR GREEN ETHYL LACTATE IV: ENZYMIC ESTERIFICATION AND OVERALL PLANT ASSESSMENT

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## OBJECTIVE

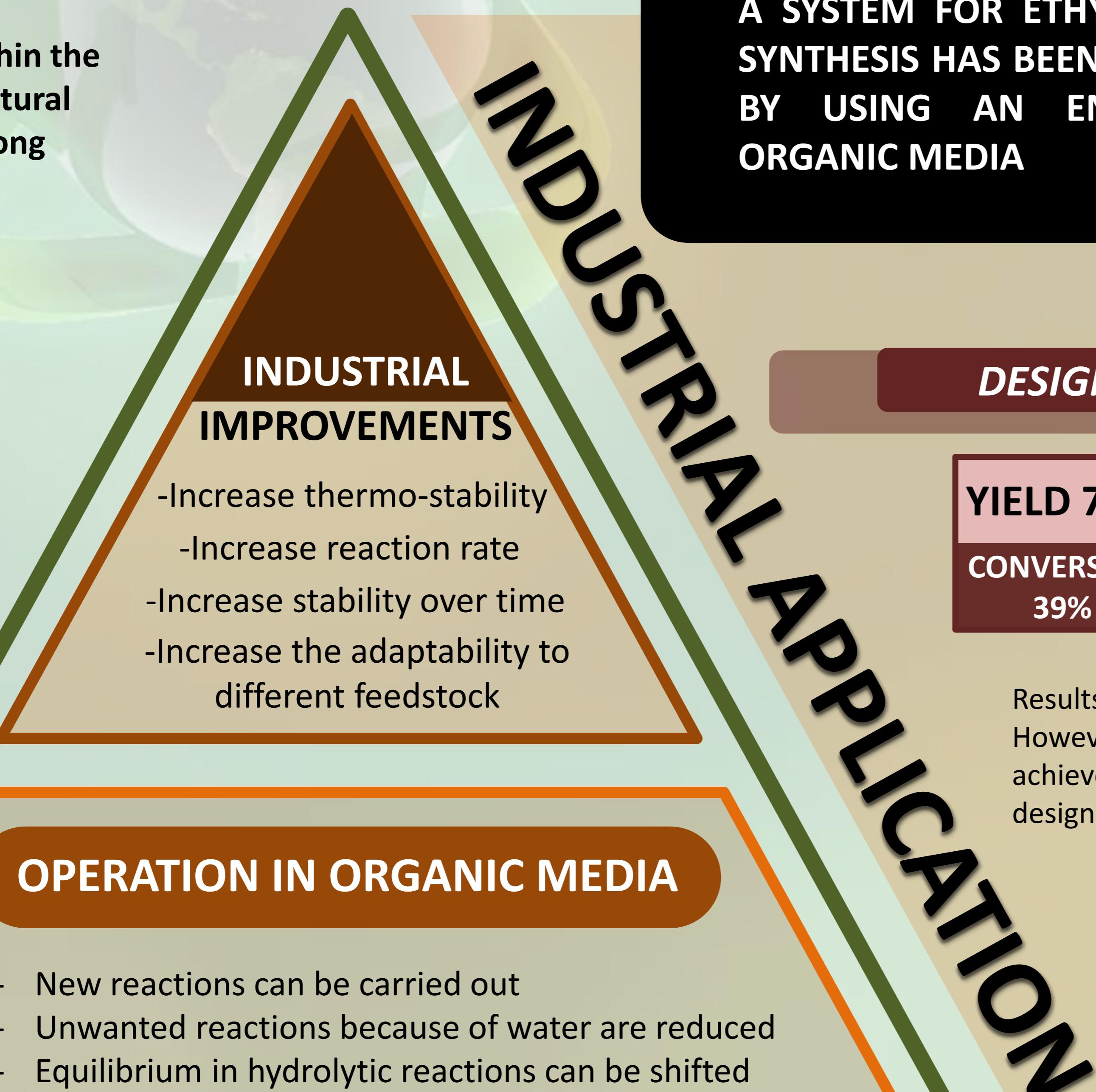
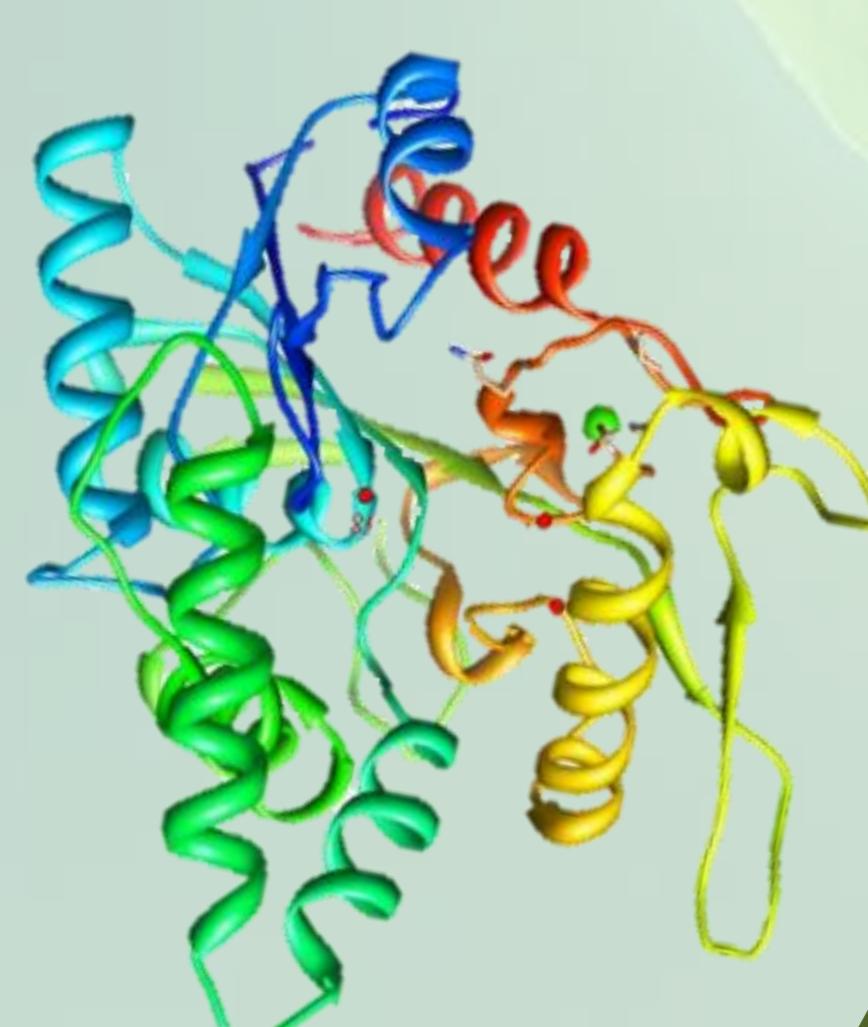
In this specific project, the esterification part of the plant has been improved and an economic analysis of the whole plant with all changes done so far has been studied in order to determine the modification effect.

### REACTIVE DISTILLATION

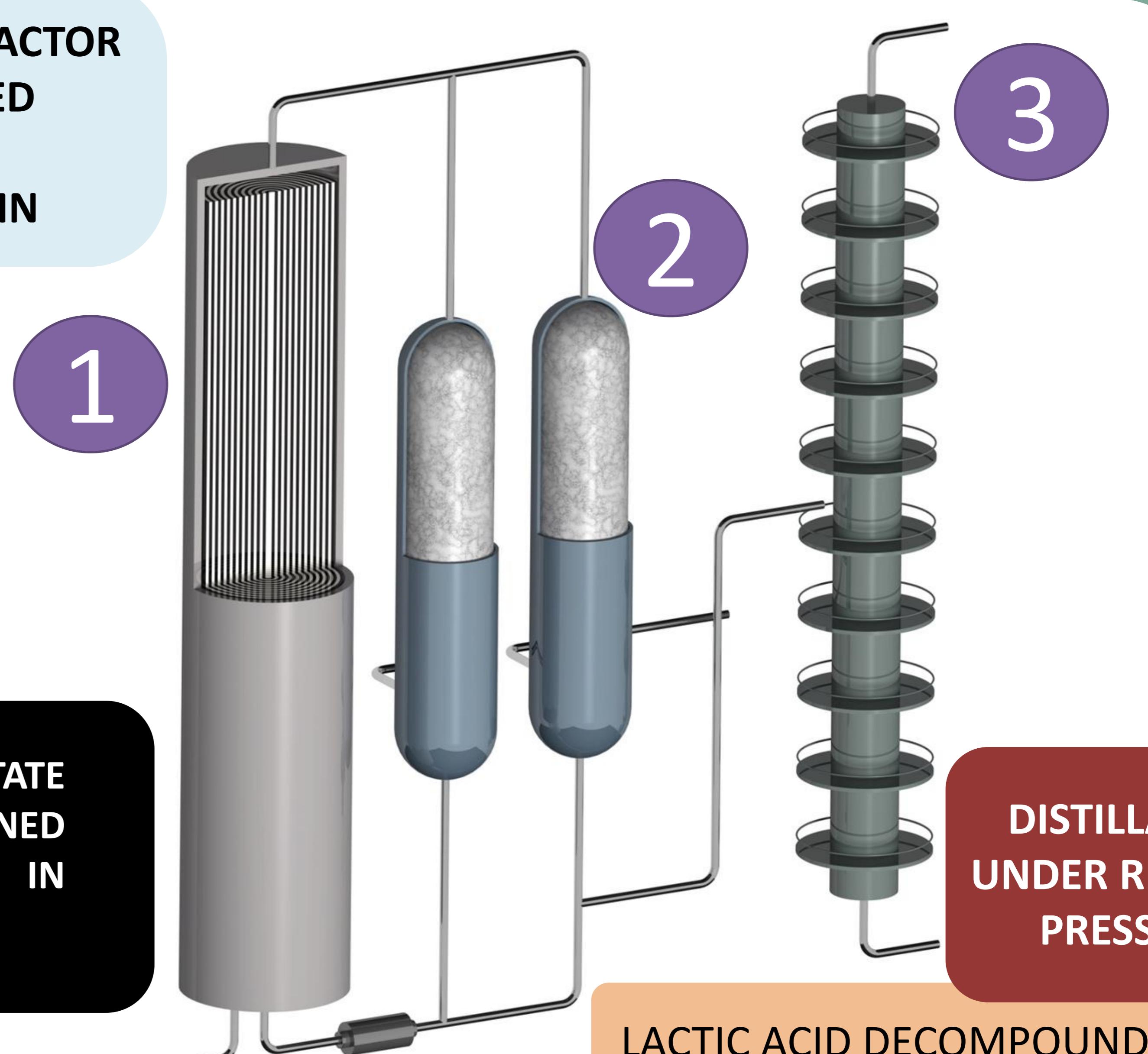
HIGH MOLAR RELATION  
LOW YIELD

### ENZYMIC ESTERIFICATION

Sub-class of enzymes within the esterase family whose natural function is to hydrolyse long chain triacylglycerol.



1- FIBROUS BED BIOREACTOR  
2- GRANULAR ACTIVATED CARBON COLUMN  
3- DISTILLATION COLUMN



3

2

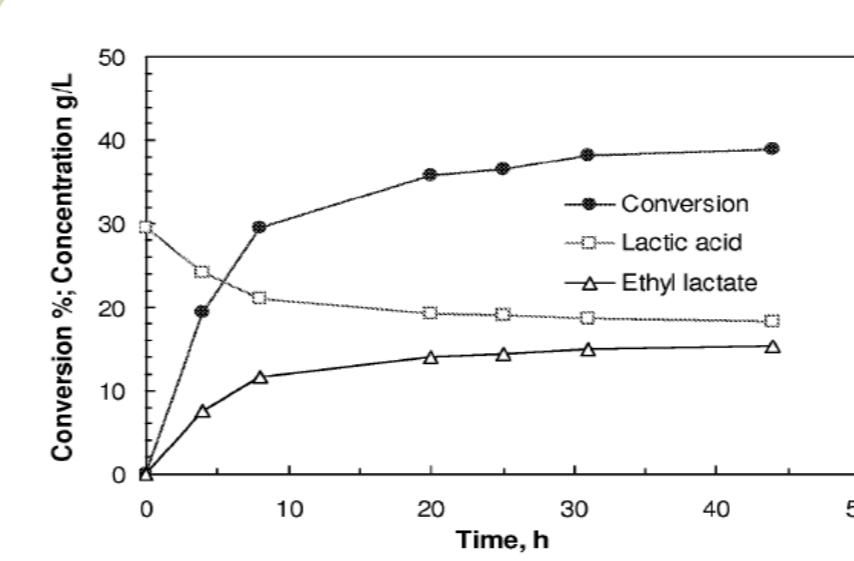
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DISTILLATION  
UNDER REDUCED  
PRESSURE

LACTIC ACID DECOMPOUNDS T°C >110°C

### DESIGN BASIS

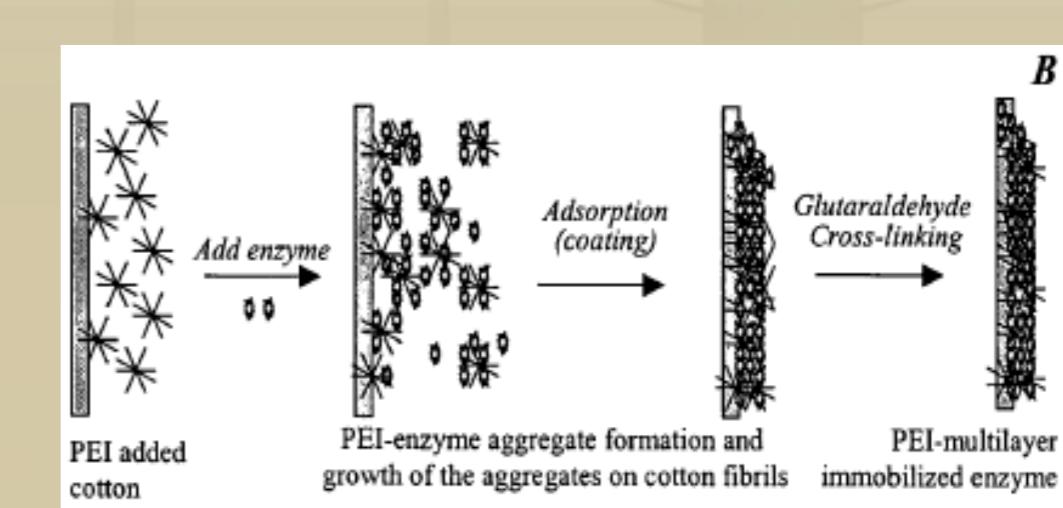
YIELD 78%  
CONVERSION  
39%



Results of the initial design are explained on this figure. However, a conversion and a yield over 90% can be achieved if a system to remove water continuously is designed.

### ENZYME IMMOBILIZATION

Enzyme will be immobilized in a packed-bed bioreactor by using cotton that surrounds a metallic structure and Polyethyleimine (PEI).

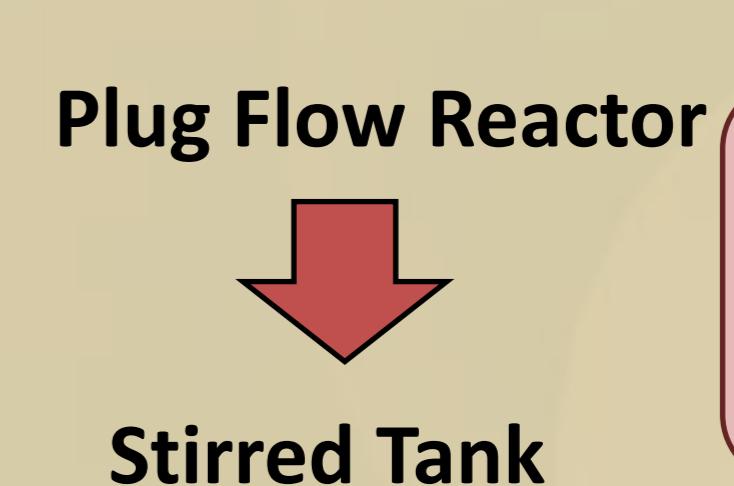


IMMOBILIZATION  
PROCEDURE

### FINAL SYSTEM DESIGN

To allow a continuous water extraction, it has been considered that a differential part of the fluid will remain in the system by doing 10 turns around the system before it continuous the process.

### 1. WATER CONTINUOUSLY REMOVED: Conversion 90%



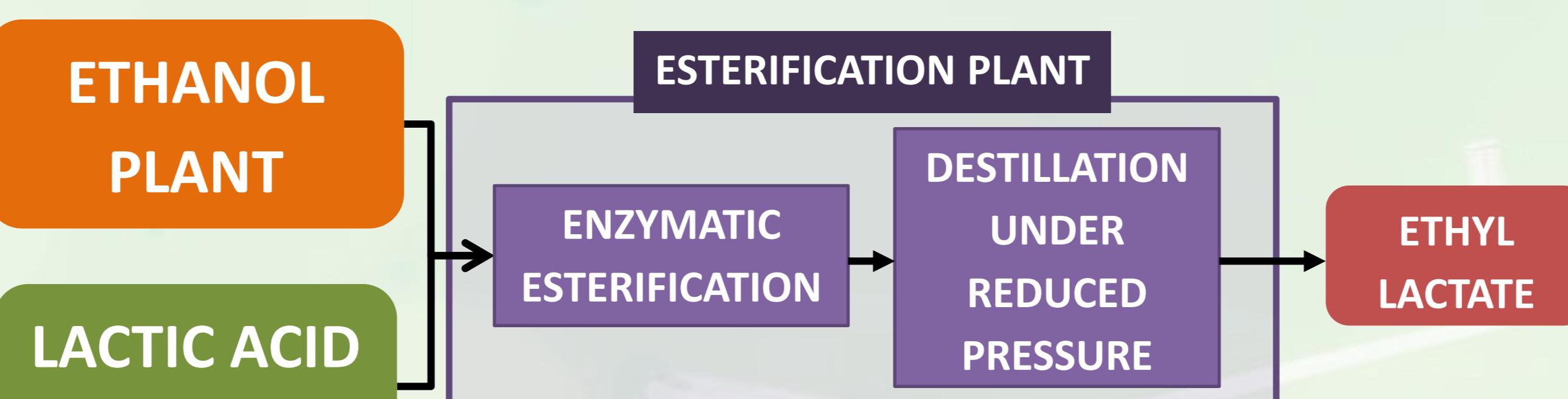
EASIER TO  
CONTROL

### 2. UNIFORM REACTION SYSTEM (Recirculation)

THIS SYSTEM WILL BE CHEAPER AND SAFER

## PLANT DIAGRAM

After all the improvements done, the plant has now a more linear evolution. Using two different feedstock enabled us to optimize each plant separately. This and the efficiency esterification improvement presents us a more operationally simple plant that can be economically attractive

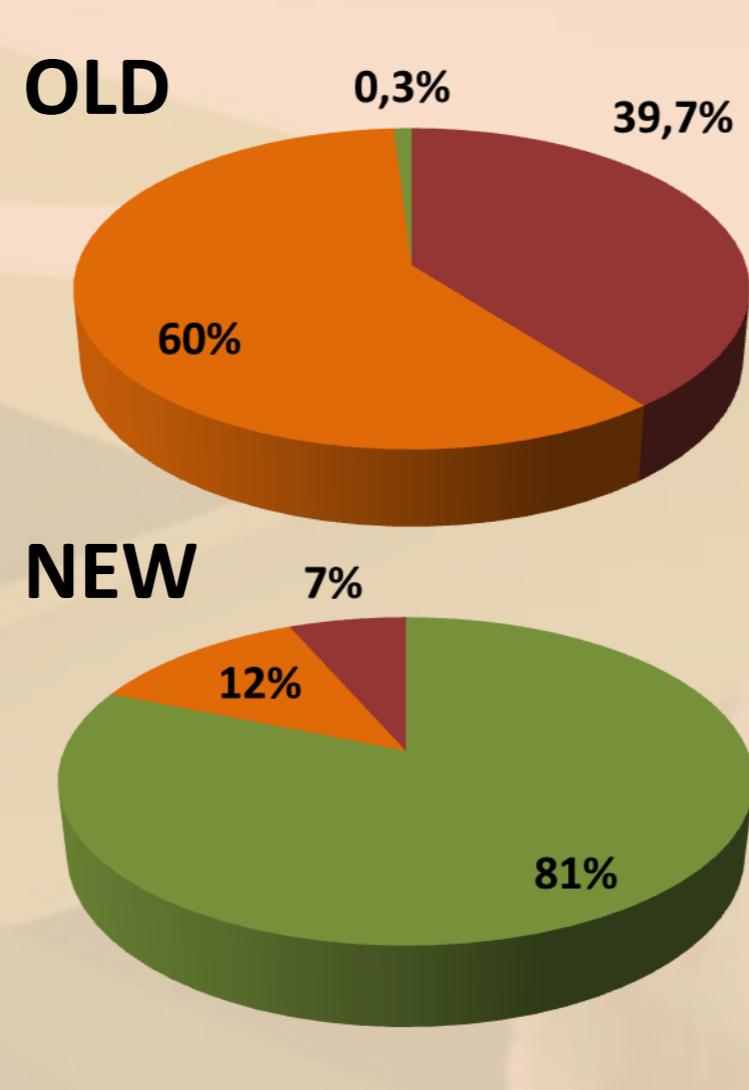


## ECONOMIC ANALYSIS

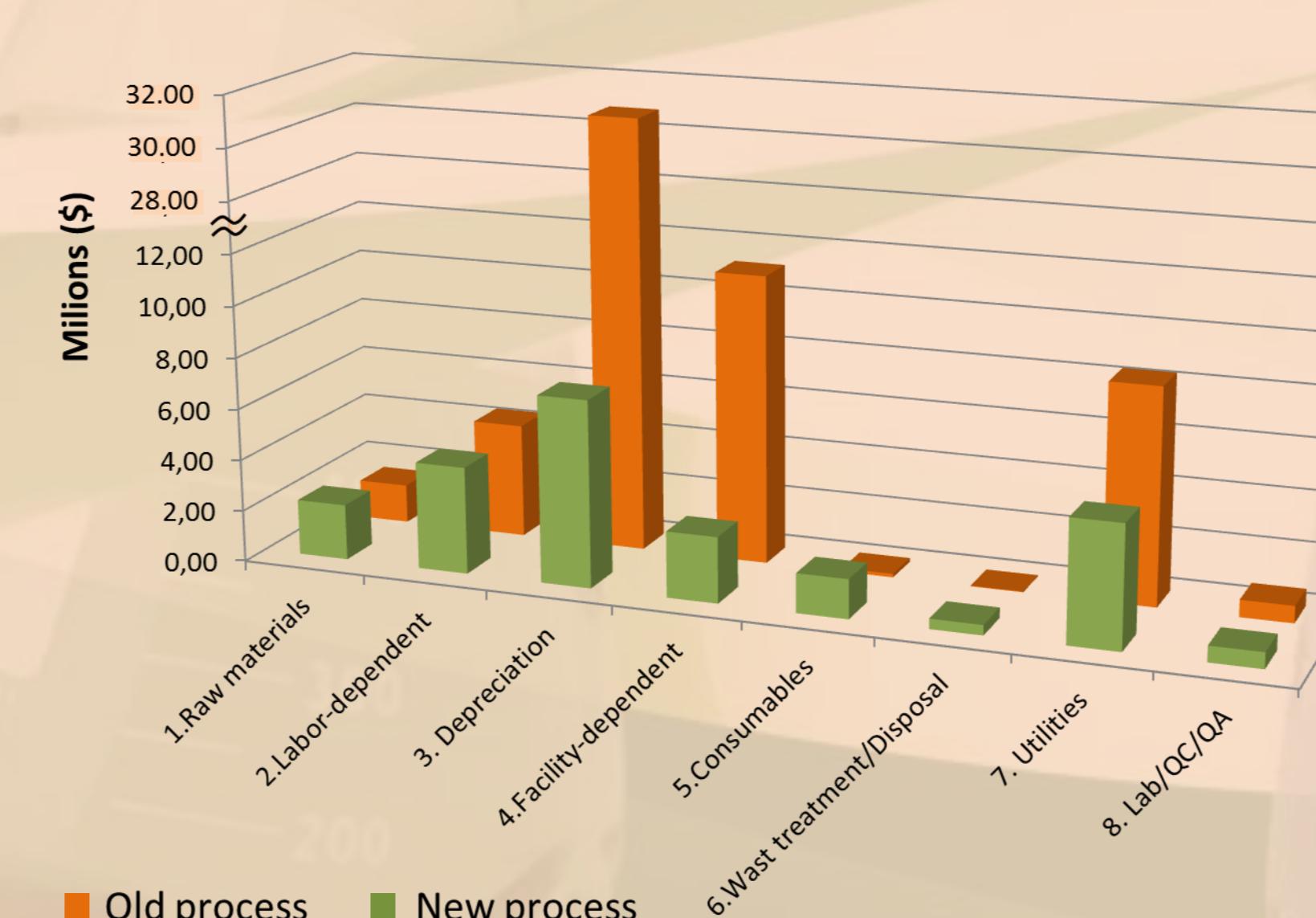
	OLD	NEW	
Income	64	44	M\$/year
Net profit (30% tax)	4	14	M\$/year
ROI	0,64	9,67	%
Pay Back Return	18,16	6,88	Years
VAN	-254	50	M\$
Unitary Cost	5,84	2,34	€/Kg

OBJECTIVE  
ACHIEVED

- Direct fix cost and initial inversion reduction. Now esterification has the main role when it comes to the DFC cost. However, despite the increase, the process efficiency compensates the increment.
- Increase in the raw material and consumable cost. The plant is now more variable cost dependent.



DIRECT FIX CAPITAL

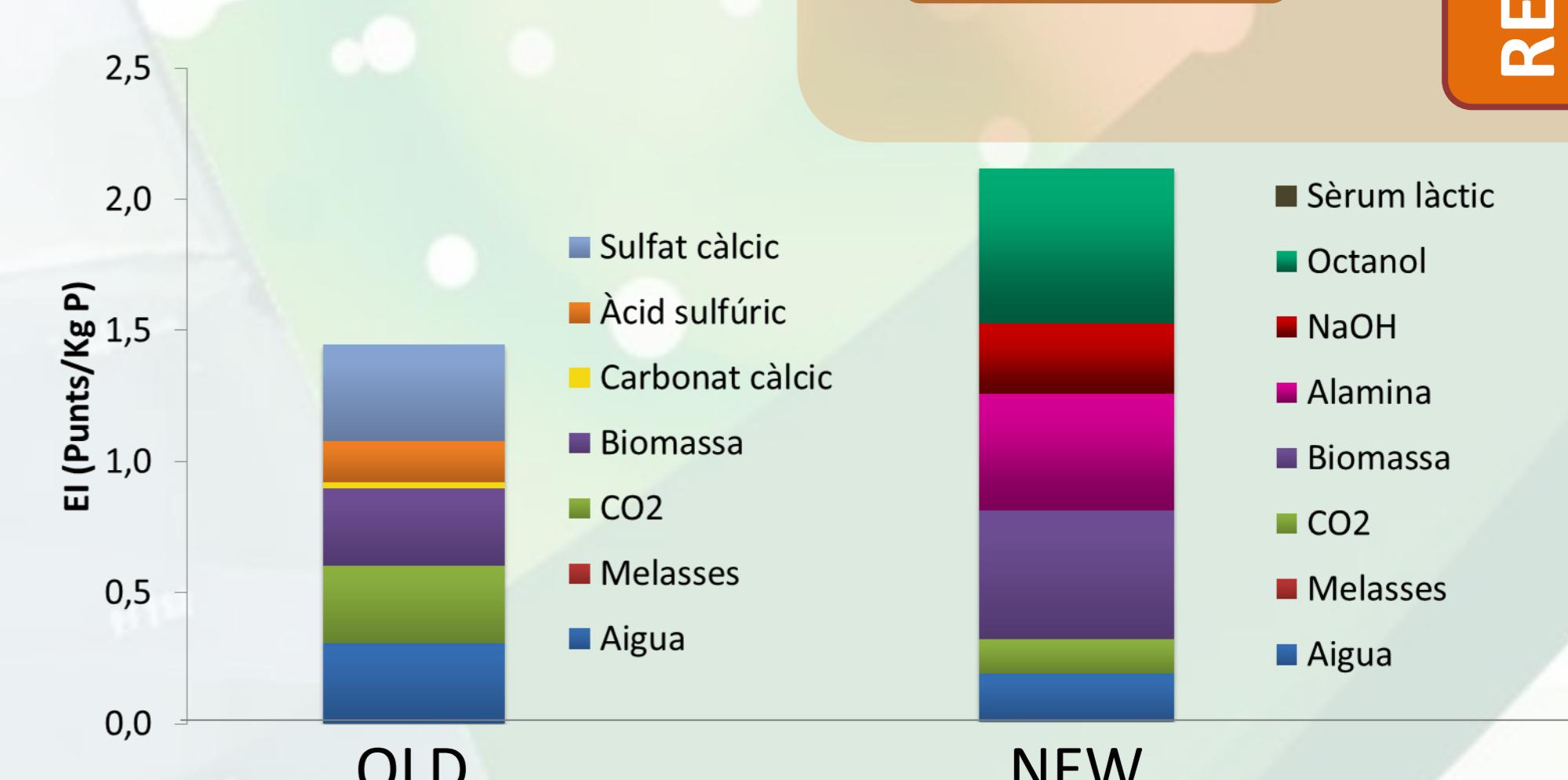


ANNUAL PLANT COST

## ENVIRONMENTAL ANALYSIS

THE TOTAL ENVIRONMENTAL INDEX OF THE PLANT IS NEARLY THE SAME AND IS FAR AWAY FROM THE ONES OBTAINED BY THE CHEMICAL INDUSTRY (>10).

OBJECTIVE  
ACHIEVED



Products with high environmental index (calcic sulphate and calcic carbonate) have been removed in the lactic acid plant. However, new more dangerous products (Alamine and Octanol) have been introduced. The clue to success is the recirculation of these organic solvents, which allow us to have almost the same total environmental index.

## CONCLUSION

After all the improvements done in the whole plant, a project that initially was not economically attractive is now a good opportunity for investors while at the same time the plant design is environmentally friendly.

## REFERENCES

- Yang, S-T.(2013), Patent US 8.357.519. United States
- Yang, S-T., Albayrak, N. (2007). Patent US 7.166.451. United States
- Tufvesson, P., "Lipase Catalysed Synthesis of Speciality Chemicals. Technical, economical and environmental aspects", Department of Biotechnology, Lund University, December 2008.