
This is the **published version** of the bachelor thesis:

Almozara García, Andrés; Gasset Franch, Arnau; Llimos Turet, Jordi; [et al.].
Design of a slurry treatment plant and biocombustible production : part III,
module tertiary treatment and biocombustible production. 2016. 1 pag. (815
Graduat o Graduada en Biotecnologia)

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INTRODUCTION

The main purpose of the plant is to remove wastes resulting from the anaerobic digestion of pig manures. The effluents from this process are rich in nitrates and phosphates that, in excess, they become dangerous pollutants. In this paper it is proposed the use of microalgae as bioremediation organisms, since they are able to assimilate both components while consuming CO₂ and produce a valuable biomass. Given the chemical composition of the biomass, it intends to carry out an ABE fermentation, with the consequent production of acetone, n-butanol and ethanol, thus making profitable the plant costs.

- Elimination N and P from water.
- Substitution EDAR tertiary treatment.
- Production n-butanol, acetone, ethanol.
- Renewable source energy.
- Greenhouse-gas reduction (CO₂ consumption).
- Creation of sustainable production systems.

MICROALGAE CULTURE

Scenedesmus obliquus

Characteristics:

High growth rate.

Rapid elimination of N and P.

High tolerance to [N].

High consumption CO₂.

Flocculation tendency.

Proper chemical profile



20-30% Lipids
50% Carbohydrates
15% Proteins

The pig manure effluent (2 m³/day) is mixed with water coming from the secondary treatment of EDAR plant at Prat de Lluçanes (29 m³/day).

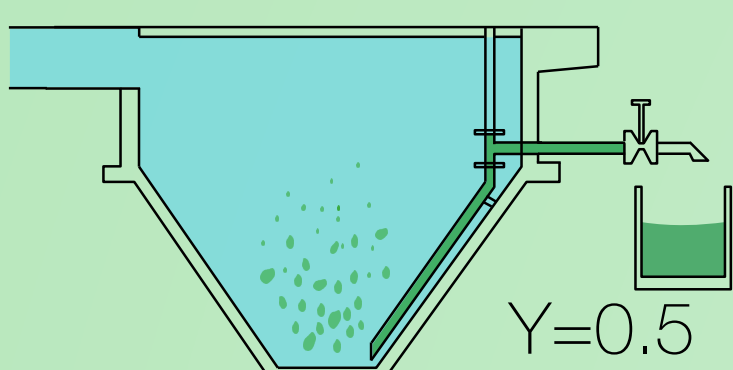
Benefits

Energy savings: Replacing the classic tertiary treatment.
Dilution of [N]: inhibition is minimized.
The turbidity of pig manure decreases: better light penetration

MICROALGAE RECOVERY

Sedimentation

Flocculation favoured by the addition of Al₂(SO₄)₃.



Y=0.5

Disck centrifuge

Biomass concentration of 30 (g/l)

Flow = 10 m³/day

	Nitrogen total (mg/l)	Phosphorus total (mg/l)	Ratio N/P
Initial flow	230	32,6	15,65
F. Section 1	198	28,3	15,5
F. Section 2	167	24	15,4
F. Section 3	135	19,7	15,2
F. Section 4	104	15,4	15
F. Section 5	72	11	14,5
F. Section 6	41	6,8	13,4
Final flow	9,4	2	-

7 sections

3.6 hectares extension

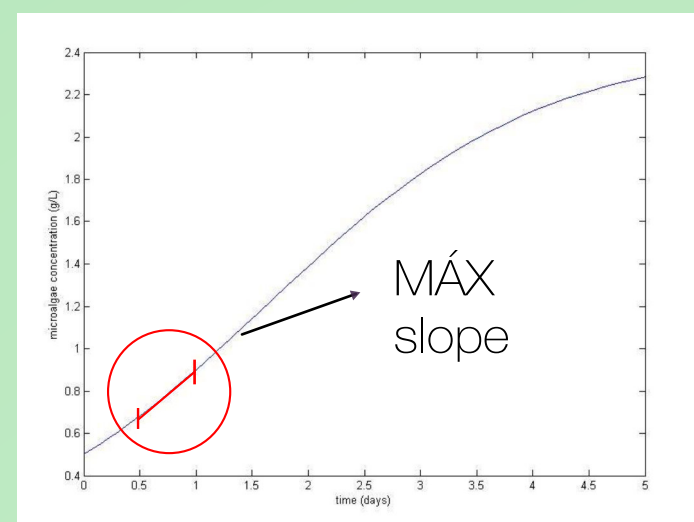
Productivity 3.65 g/l·day

Production of 2715 kg/day

CULTIVATION MODE

CCS: Channels conected in serie

Growth simulation



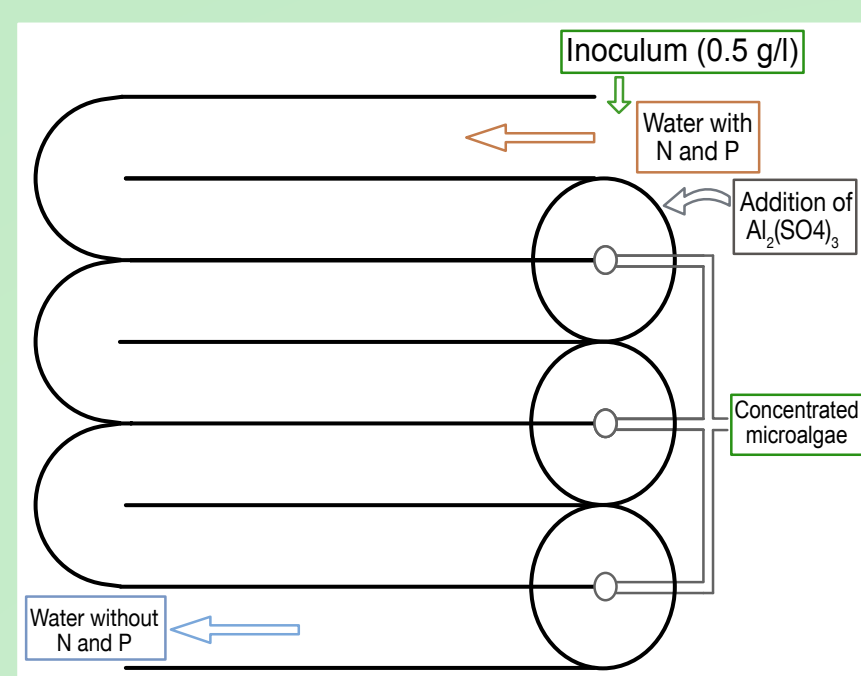
$$\frac{dX}{dt} = \mu_{max} X \left(1 - \frac{X}{X_{max}}\right)$$

Ratio optimization N/P(15)
Optimization of intervals growth (0.5-1 g)

Characteristics:

Depth 25 cm
Low cost system
Robustness against temperature changes
Analog flow to RCFP
In each section are recovered [X]₀=0.5 g/l

Scheme CCS



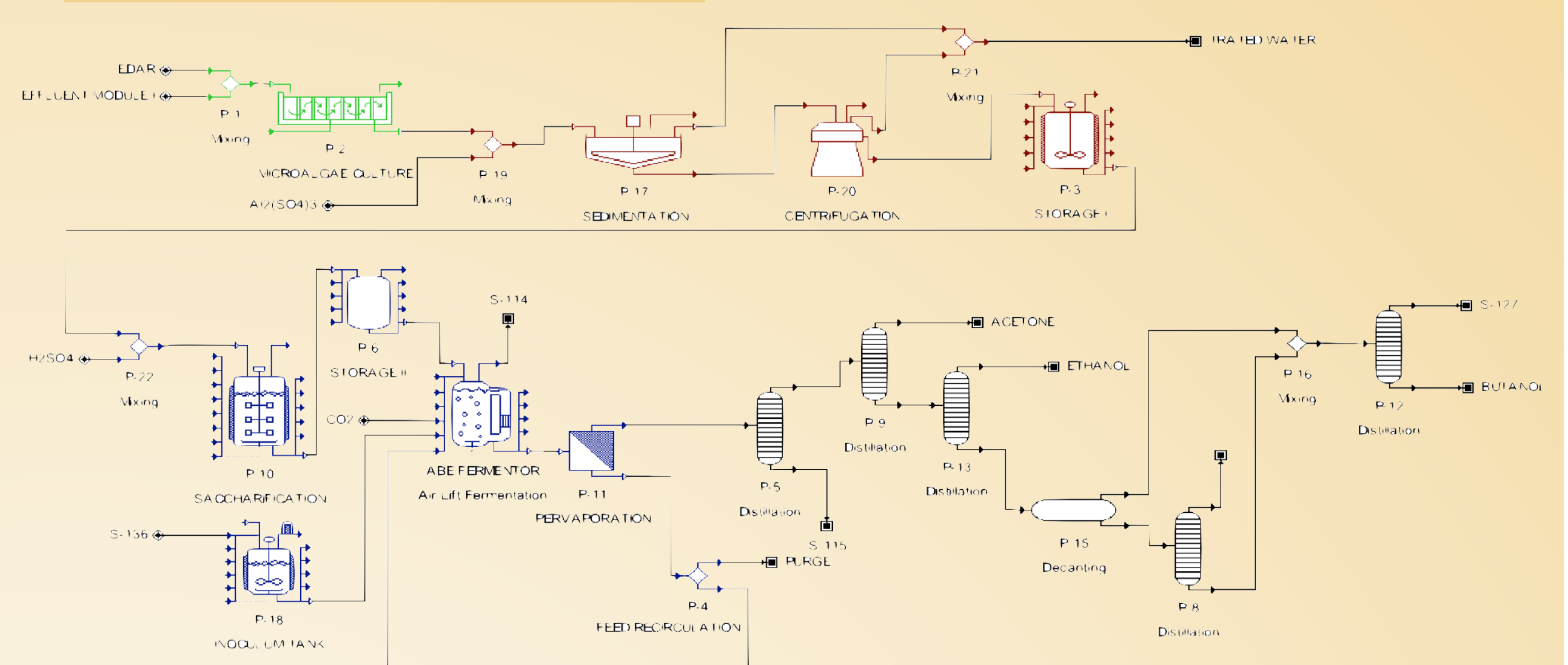
Advantages

Inhibition is limited to the first section (230 ppm N)

Last section are stressed by nutrient deficiency: lipids production is stimulated

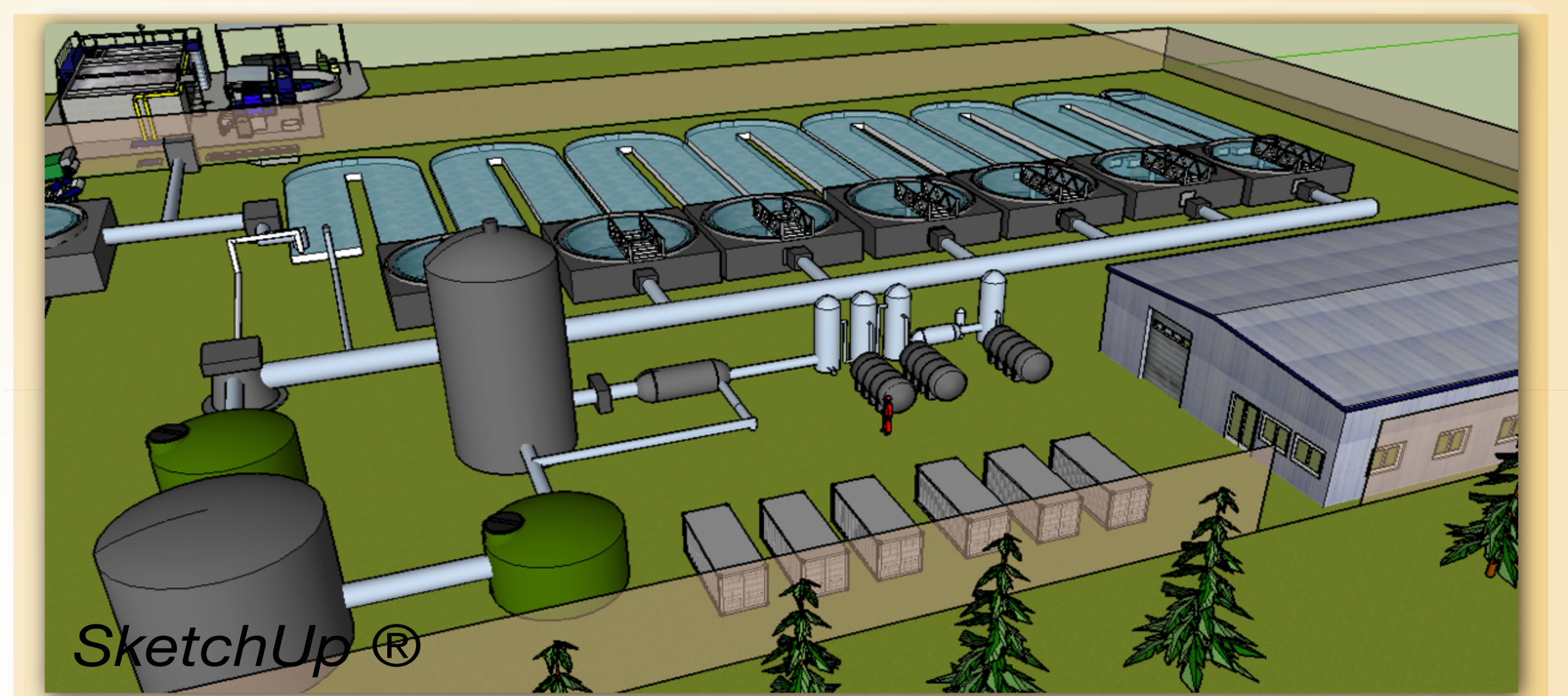


FLOW DIAGRAM



SuperPro Designer®

LAYOUT



ECONOMIC ANALYSIS

TCI = 7.175 M €

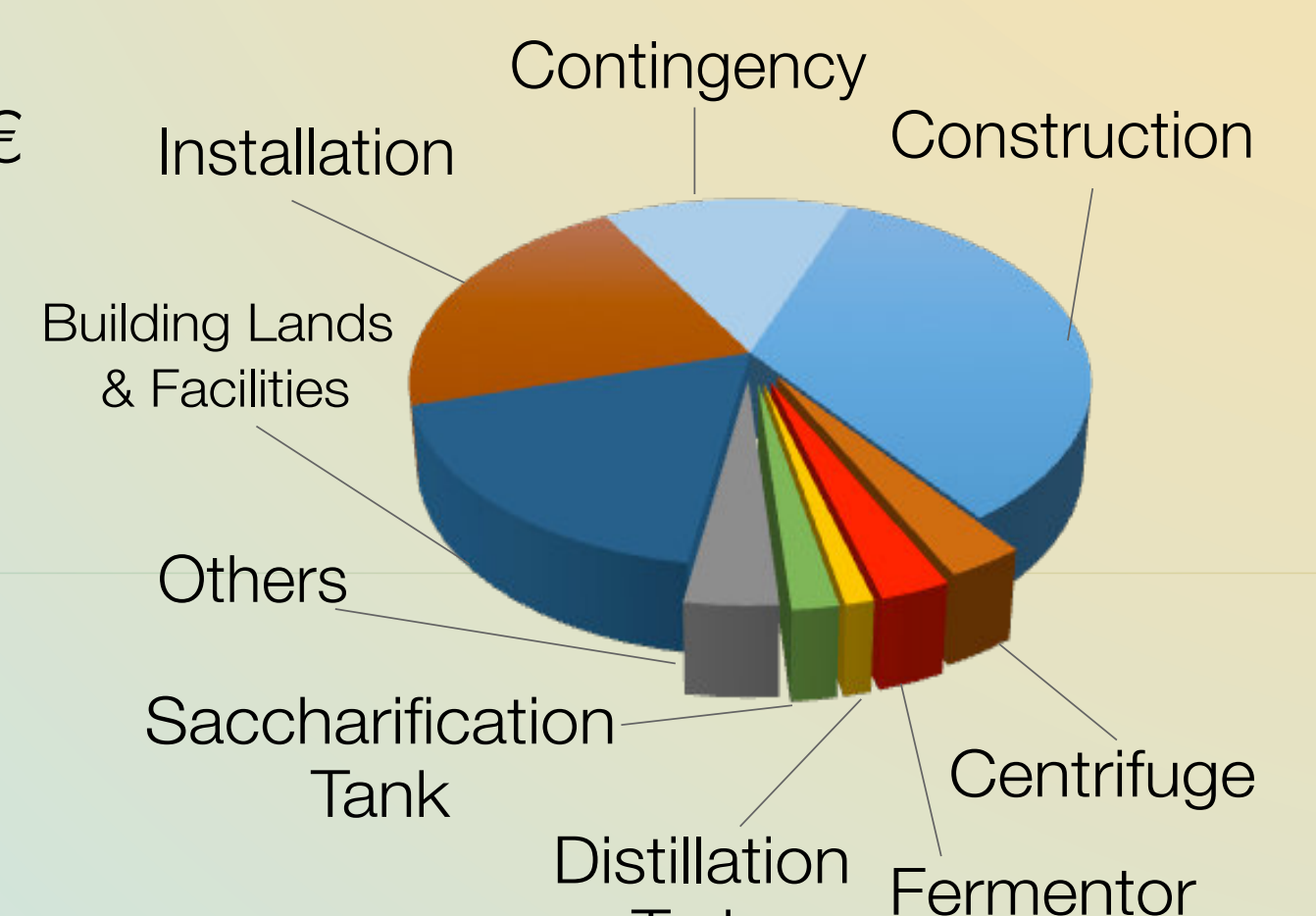
Annual operating cost = 0.43 M €

→ 6 Operators

Revenues = 0.777 M €

ROI = 4.9%

Total capital investement



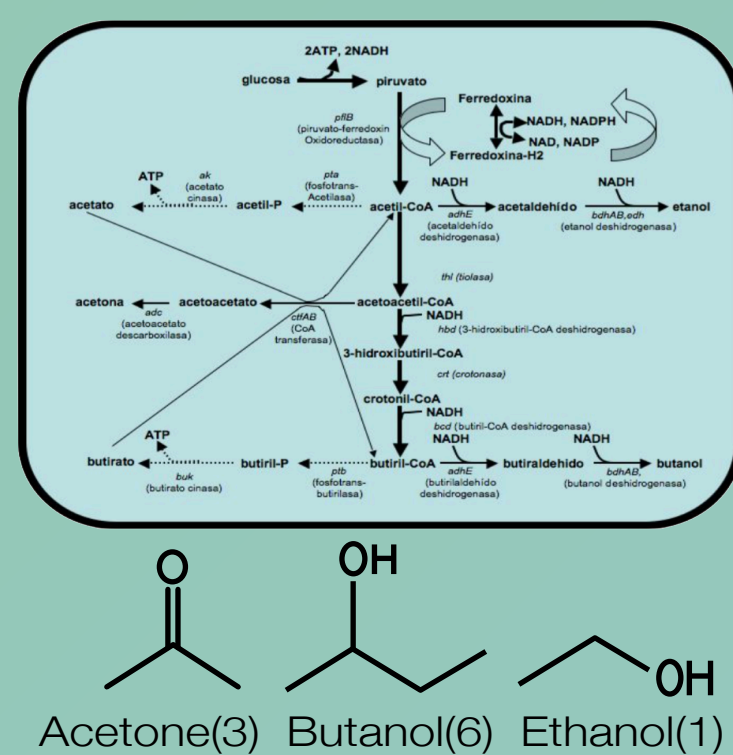
Annual net profit of 390 000 €

ABE FERMENTATION

Clostridium acetobutylicum

Characteristics

Gram positive
Strict anaerobe
Degradation of sugars, starch, protein and cellulose



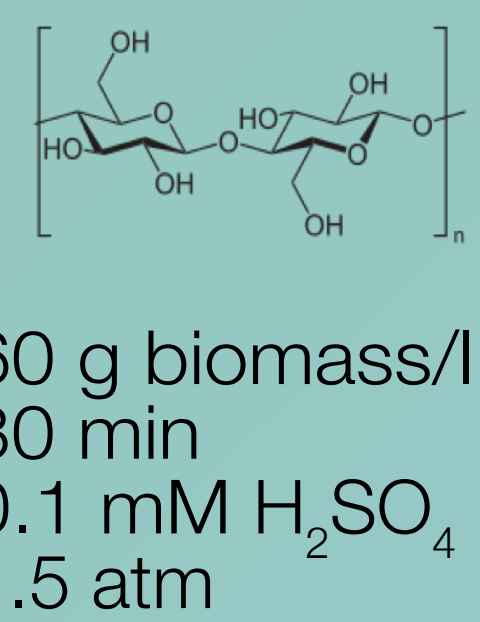
Acetone(3) Butanol(6) Ethanol(1)

TERMAL SACCHARIFICATION

Operating conditions

V_{reactor} = 11 m³
5 cycles per day at 82% load
Y = 0.5 (g sugar/g algae)

Obtaining solubles sugar



CULTIVATION MODE

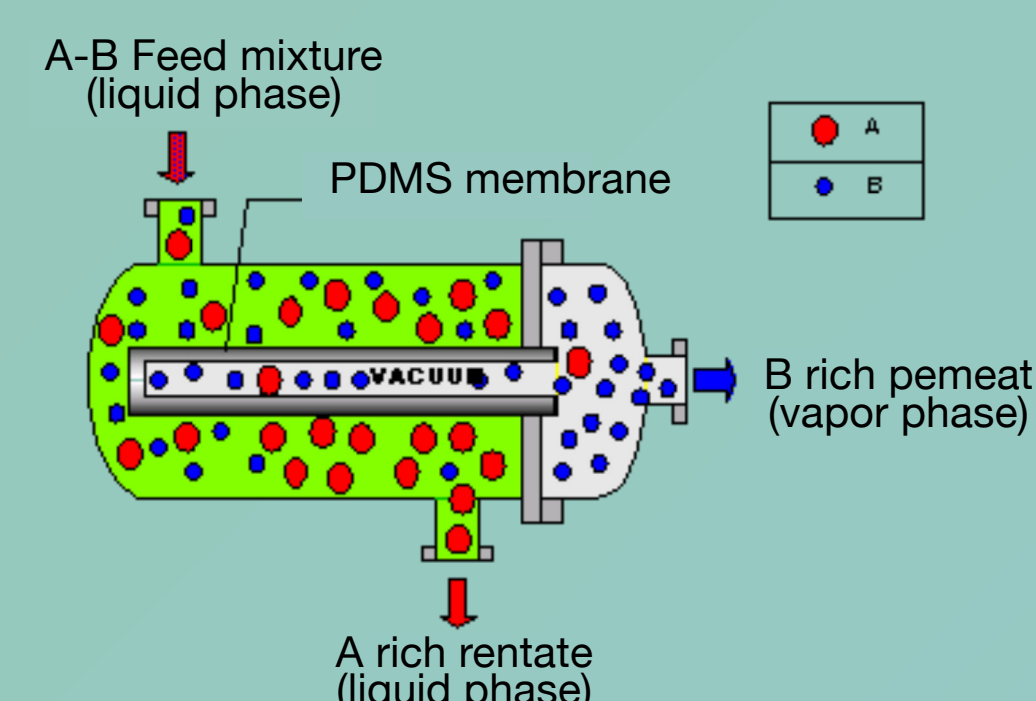
Air-lift operating in semi-continuous (140 m³)

Immobilized cells in polyvinyl-cryogel support

Pervaporation chamber in situ: Membrane PDMS

Homogeneous distribution of inhibitory compounds

Elimination of inhibitory compounds



Butanol = 424 T/year
Acetona = 69 T/year
Ethanol = 23 T/year

DOWNSTREAM

Distillation train

Butanol 99.7%

Acetona 99.5%

Ethanol 96 %



Reduction of 50% of total consumption compared to conventional technology

ENVIRONMENTAL ANALYSIS

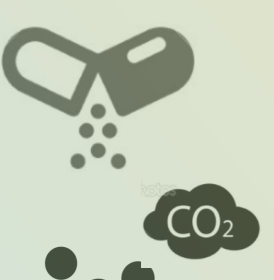
Elimination of N and P: Neither eutrophication nor ground water leaching

Bioremediation of pharmaceutical drugs in water

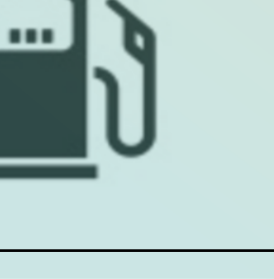
Reducing emissions of greenhouse gases: 1460 T CO₂/year

Sustainable Fertilizers Production

Energy production from renewable sources



250 people



Autonomy of the area is stimulated

22.5 T/year
470 m³/year gasoline equivalent

CONCLUSIONS

A serious environmental problem is solved effectively and sustainably. The use of microalgae as bioremediation system proves to be very effective and potentially applicable. ABE fermentation, as a strategy of biomass revaluation and production of biofuels, has many advantages but it must overcome some technical obstacles.

- Avoid formation of biofilms: Use of closed systems cultivation.
→ Reduction of land needed
- Butanol is high energy biofuel and it's not corrosive for engines.
- Use of engineering clostridium strains.
- Improvement of ABE products recovery systems.

Bibliography

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